

WHAT IS CLAIMED IS:

1. A method for producing virus inactivated human gammaglobulin G, which method comprises:
- 5 (a) suspending a precipitate of IgG in an aqueous solution containing a carbohydrate;
- (b) reducing the content of contaminants in the suspension with PEG;
- 10 (c) applying the suspension to an anionic exchange resin in column to obtain an effluent;
- (d) subjecting the effluent to ultrafiltration so that the content of PEG in said effluent is reduced;
- 15 (e) viral inactivation of the filtered effluent by at least one method selected from the group consisting of (i) pasteurisation and (ii) treatment with solvent/detergent; and
- (f) precipitating and washing the virus inactivated human gammaglobulin G from the viral inactivated effluent.
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2. A method for producing virus inactivated human gammaglobulin G according to claim 1, wherein the precipitate of IgG is obtained or provided by
- 25 fractionation of human plasma with ethanol.
3. A method for producing virus inactivated human gammaglobulin G according to claim 2, wherein the precipitate of IgG comprises fractions II+III of the
- 30 Cohn method.

4. A method for producing virus inactivated human gammaglobulin G according to claim 1, wherein the carbohydrate is a sugar-alcohol.
- 5 5. A method for producing virus inactivated human gammaglobulin G according to claim 4, wherein the sugar-alcohol is sorbitol.
- 10 6. A method for producing virus inactivated human gammaglobulin G according to claim 4, wherein the sugar-alcohol is present at a concentration of between 2% and 10% (w/v).
- 15 7. A method for producing virus inactivated human gammaglobulin G according to claim 1, in which the step of reducing the concentration of contaminants in the suspension is performed with PEG at a concentration from 2.5% to 5.5% (w/w) and at a pH from 4.8 to 5.5.
- 20 8. A method for producing virus inactivated human gammaglobulin G according to claim 1, wherein the pH of the suspension is between 5.7 and 6.3 when applied to the anionic exchange resin column.
- 25 9. A method for producing virus inactivated human gammaglobulin G according to claim 1, wherein the anionic exchange resin column:
- 30 (a) Contains DEAE-agarose resins, and
(b) Admits a charge of between 1 g and 2.5 g of fraction II+III per ml of resins.

10. A method for producing virus inactivated human
gammaglobulin G according to claim 1, in which the
effluent is subjected to ultrafiltration through a
5 membrane of 100 kDa nominal molecular cut-off.
11. A method for producing virus inactivated human
gammaglobulin G according to claim 10 in which,
after said step of ultrafiltration, the effluent is
10 diafiltered against a solution containing a sugar
alcohol.
12. A method for producing virus inactivated human
gammaglobulin G according to claim 11, in which the
15 sugar alcohol is sorbitol.
13. A method for producing virus inactivated human
gammaglobulin G according to claim 11, in which the
sugar alcohol is present in solution at a
20 concentration between 2% and 10% (w/v).
14. A method for producing virus inactivated human
gammaglobulin G according to claim 11, in which said
diafiltration is performed at a pH between 4.0 and
25 4.8.
15. A method for producing virus inactivated human
gammaglobulin G according to claim 11, in which said
diafiltration is performed with a transmembrane
30 pressure below 1.2 bar.

16. A method for producing virus inactivated human
gammaglobulin G according to claim 1 further
comprising, prior to the step of viral inactivation,
a step of treating the filtered effluent at an acid
pH.
17. A method for producing virus inactivated human
gammaglobulin G according to claim 16, wherein said
step of treating the filtered effluent at an acid pH
is carried out in the presence of a sugar-alcohol at
a pH of 3.95 to 4.05 and at a temperature of 35 to
38 °C from 1 to 4 hours.
18. A method for the production of virus-inactivated
human gammaglobulin G according to claim 17 in which
the sugar-alcohol is sorbitol, said sorbitol being
present at a concentration between 2% and 10% (w/v).
19. A method for the production of virus-inactivated
human gammaglobulin G according to claim 1, wherein
viral inactivation comprises pasteurisation of the
filtered effluent.
20. A method for the production of virus-inactivated
human gammaglobulin G according to claim 19 in which
the filtered effluent is pasteurized in the presence
of a sugar alcohol.
21. A method for the production of virus-inactivated
human gammaglobulin G according to claim 19, wherein
the sugar alcohol is sorbitol.

22. A method for the production of virus-inactivated human gammaglobulin G according to claim 20 in which the sugar alcohol is present at a concentration of between 25% and 35% (w/w).
23. A method for the production of virus-inactivated human gammaglobulin G according to claim 20 in which the filtered effluent is treated with solvent/detergent after said pasteurisation.
24. A method for the production of virus-inactivated human gammaglobulin G according to claim 23 in which, before said treatment with solvent/detergent, the pasteurised effluent is diluted with water for injection so that:
- (a) the concentration of sugar alcohol is 25% (w/w) or less, and
 - (b) the concentration of protein is between 1% and 3% (w/v).
25. A method for the production of virus-inactivated human gammaglobulin G according to claim 1, wherein viral inactivation comprises treatment with solvent/detergent.
26. A method for the production of virus-inactivated human gammaglobulin G according to claim 25 in which, after treatment with said solvent/detergent, the effluent is diluted with water for injection so that the pH is adjusted to between 7.0 and 9.0.

27. A method for the production of virus-inactivated human gammaglobulin G according to claim 26, wherein the pH is adjusted to between 7.8 and 8.4.
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28. A method for the production of virus-inactivated human gammaglobulin G according to claim 26 in which the effluent is diluted by adding, for each kilogram of effluent, between 1-2 kg of water for injection.
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29. A method for the production of virus-inactivated human gammaglobulin G according to claim 1 in which the virus inactivated human gammaglobulin G is precipitated from the virus inactivated effluent by the addition of PEG.
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30. A method for the production of virus-inactivated human gammaglobulin G according to claim 29 in which PEG is added to the virus inactivated effluent to a final concentration between 12% and 17% (w/w).
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31. A method for the production of virus-inactivated human gammaglobulin G according to claim 29, in which the precipitated human gammaglobulin G is separated on a tangential flow filtration membrane.
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32. A method for the production of virus-inactivated human gammaglobulin G according to claim 31, in which the tangential flow filtration membrane has a pore size from 0.1 to 0.45 microns.
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33. A method for the production of virus-inactivated human gammaglobulin G according to claim 31 wherein the precipitate is washed in said tangential flow filtration membrane.
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34. A method for the production of virus-inactivated human gammaglobulin G according to claim 33, in which the precipitate is washed by the addition of four or more volumes of solution used to precipitate the virus inactivated human gammaglobulin G.
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35. A method for the production of virus-inactivated human gammaglobulin G according to claim 29 wherein the precipitated virus inactivated human gammaglobulin G is solubilized by the addition of an acid solution at pH below 5.5, which acid solution contains a carbohydrate.
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36. A method for the production of virus-inactivated human gammaglobulin G according to claim 35 wherein the acid solution comprises acetic acid with an adjusted concentration of between 1 mM to 10 mM.
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37. A method for the production of virus-inactivated human gammaglobulin G according to claim 35 wherein the carbohydrate comprises a sugar alcohol.
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38. A method for the production of virus-inactivated human gammaglobulin G according to claim 37, in which the sugar alcohol is present at a concentration from 5-20% (w/w).
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39. A method for the production of virus-inactivated human gammaglobulin G according to claim 35 wherein said acid solution is adjusted with an alkali to pH 4.0-4.5.
40. A method for the production of virus-inactivated human gammaglobulin G according to claim 35, in which the amount of acid solution added is such that the concentration of PEG in the solubilized human gammaglobulin G is from 2% to 4% (w/w).
41. A method for the production of virus-inactivated human gammaglobulin G according to claim 40, in which the concentration of PEG in the solubilized human gammaglobulin G is from 2.8% to 3.4% (w/w).
42. A method for the production of virus-inactivated human gammaglobulin G according to claim 35, further comprising steps of:
- (a) adding an alkali to the acid solution so that the pH is adjusted to between 7.5 and 8.5, and
 - (b) precipitating and separating insoluble high molecular weight aggregates from the pH adjusted solution.
43. A method for the production of virus-inactivated human gammaglobulin G according to claim 42, wherein insoluble high molecular weight aggregates are separated from the pH adjusted solution by filtration.

- 5 44. A method for the production of virus-inactivated human gammaglobulin G according to claim 42 further comprising, after separating insoluble high molecular weight aggregates from the pH adjusted solution, diafiltration and concentration of the solution through ultrafiltration membranes of 100 kDa nominal molecular cut-off and at a transmembrane pressure below 1.2 bar.
- 10 45. A method for the production of virus-inactivated human gammaglobulin G according to claim 44, wherein the solution is concentrated to a protein concentration of 1% to 3% (w/v).
- 15 46. A method for the production of virus-inactivated human gammaglobulin G according to claim 44, further comprising steps of:
- 20 (a) heating the solution to between 20 and 25 °C; and
- (b) nanofiltration of the solution through membranes having a nominal pore size of 50 nm or less.
- 25 47. A method for producing virus inactivated human gammaglobulin G according to claim 46 wherein the membranes have a nominal pore size of approximately 20 nm.
- 30 48. A virus-inactivated human gammaglobulin G manufactured according to the process set forth in claim 1.